
REFRIGERATION SCIENCE AND TECHNOLOGY PROCEEDINGS

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PROCEEDINGS

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Contents

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CONTENT

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001	POTENTIAL OF CO ₂ /HFOS MIXTURES APPLIED IN AIR SOURCE HEAT PUMP FOR DHW PRODUCTION	7
	<i>Fang Zhou, Jian Liu, Xiaosong Zhang</i>	
0002	INFLUENCE OF SUBCOOLING IN R449A SUPERMARKET LOWTEMPERATURE REFRIGERATION CIRCUIT USING MEDIUM TEMPERATURE COOLING LOAD	15
	<i>Adrián Mota Babiloni, Pau Giménez Prades, Cosmin Mihai Udrouiu, Ángel Barragán Cervera, Joaquín Navarro Esbrí</i>	
0003	REFRIGERANT CHARGE STUDY FOR R454C AS A REPLACEMENT FOR R410A IN A RESIDENTIAL HEAT PUMP SPLIT SYSTEM	22
	<i>Weigang Hou, Hafez Raeisi Fard, Larry Burns, Eckhard A. Groll, James E. Braun, Davide Ziviani</i>	
0004	NOVELREFRIGERANTR-474AFORAUTOMOTIVEHEATPUMPAPPLICATIONS	31
	<i>Daisuke KARUBE, Tsubasa NAKAUE, Tatsumi TSUCHIYA, Kenji GOBO, Shohei AJIOKA, Yasufu YAMADA, Yasutaka NEGISHI, Ivan RYDKIN, Álvaro de LEÓNALLUÉ</i>	
0005	A SEMI-SUPERVISED DATA-DRIVEN APPROACH FOR CHILLER REFRIGERANT LEAKAGE DETECTION	39
	<i>ZhanhuiFeng, Li Wang, Xiaokui Ma, Zhanhong Jiang, Baojun Chang</i>	
0006	MATERIAL COMPATIBILITY OF NEW LOW GWP REFRIGERANTS FOR ELECTRIC VEHICLE AIR CONDITIONING	47
	<i>Tianhao WANG, Xiaoye DAI, Lin SHI</i>	
0007	SOLUBILITIES OF R513A IN POLYOL ESTER LUBRICATING OIL AT TEMPERATURES FROM 273.15 K TO 353.15 K	54
	<i>Yubo Chen, Zhao Yang, Yong Zhang, Dongdong Jiang, Hongxia He</i>	
0008	THE MELTING POINTS AND ENTHALPY OF MELTING OF REFRIGERANTS INCLUDING HFOS AND HCFOS	61
	<i>Xian Wang, Kun Wang, Yanxing Zhao, Xueqiang Dong, Maoqiong Gong</i>	
0009	PERFORMANCE ANALYSIS OF A COMBINED COOLING AND HEATING CO ₂ SYSTEM BASED ON EJECTOR AND DEDICATED MECHANICAL SUBCOOLING	69
	<i>Baomin Dai, Ruirui Zhao, Shengchun Liu, Chen Liu, Xinhai Li, Jia Liu, Ziang Kong, Qiang Guo</i>	
0010	PERFORMANCE ANALYSIS OF COMBINED COOLING AND HEATING CO ₂ SYSTEM WITH MECHANICAL SUBCOOLING SYSTEM USING ZEOTROPIC MIXTURE AS WORKING FLUID	76
	<i>Baomin Dai, Qilong Wang, Shengchun Liu, Minghui Wang, Jianing Zhang, Fangcan Li, Xuan Zhou, Qiang Guo</i>	
0011	ENERGY AND EMISSION ANALYSIS OF CO ₂ SUPERMARKET REFRIGERATION SYSTEM	82
	<i>Shengchun Liu, Jiayu Li, Baomin Dai, Jiahao Wang, Zhao Xu</i>	
0012	EXPERIMENTAL STUDY ON SOLUBILITY OF HEXAFLUOROPROPENE(R1216) IN POLYOL ESTER LUBRICANT OIL	89
	<i>Yong Zhang, Zhao Yang, Yubo Chen, Hongxia He</i>	
0013	STUDY ON THE VAPOR-LIQUID EQUILIBRIUM OF NEW HFOS BINARY MIXED REFRIGERANT {R1234ZE(E)+R1336MZZ(E)}	97
	<i>Wei Yang, Guogeng He, Zihang Wang, Xiao Li, Zhihao Zhang</i>	
0014	ENERGY AND EXERGY ANALYSES OF AN EJECTOR-EXPANSION RECIRCULATION CYCLE WITH ZEOTROPIC MIXTURE R744/R1234YF FOR APPLICATION IN HEAT PUMPS	105
	<i>Yu Lu, Tao Bai, Jianlin Yu</i>	

0016	113
DESIGN AND INSTALLATION OF A R-454C CONDENSING UNIT, A CASE STUDY	
<i>Fabrizio Codella, Emiliano Baglioni</i>	
0017	121
SUSTAINABLE SUPERMARKET REFRIGERATION WITH HFO REFRIGERANT	
<i>Nilesh Purohit, Kaimi Gao, Patrick Birbarah, Ankit Sethi, Ryan Hulse</i>	
0018	129
PERFORMANCE ANALYSIS OF LOW GWP REFRIGERANTS IN A NOVEL DIRECT EXPANSION SOLAR ASSISTED EJECTORHEAT PUMP SYSTEM	
<i>Lingeng Zou, Ye Liu, Jianlin Yu</i>	
0019	142
CHARGE ESTIMATION OF R1243ZF/R134A FOR A CONSTANT TEMPERATURE AND HUMIDITY AIR CONDITIONER	
<i>Xi WU, Fengyi TANG, Zudi OU, Shiming XU, Xiaojing ZHU</i>	
0020	150
EXPERIMENTAL RESEARCH OF R1234yf FOR REPLACING R22 USED IN A WINDOW-TYPE AIR CONDITIONER	
<i>Tingxiang Jin, Ran Xu Zijian Lv</i>	
0021	157
THEORETICAL STUDY OF LOW GWP REFRIGERANTS IN HIGH-TEMPERATURE HEAT PUMP SYSTEMS	
<i>Fan Zhang, Zhao Feng Meng, Suiju Dong, Yin Liu, Chuangchuan Ding, Ziheng Huo, Mingming Wang</i>	
0022	164
PERFORMANCE EVALUATION OF A SINGLE-STAGE LINDE-HAMPSON REFRIGERATION SYSTEM USING LOW-GWP R1234YF-BLENDS	
<i>Yanbin Qin, Nanxi Li, Baolin Liu, Hua Zhang</i>	
0023	174
STUDY ON THE INFLUENCE OF THE SUPERHEAT OF THE ELECTRONIC EXPANSION VALVE ON THE PERFORMANCE OF THE AIR CONDITIONING SYSTEM OF THE HEAT PUMP TYPE PURE ELECTRIC BUS UNDER FROSTING CONDITION	
<i>HaiJun Li, ChaoYue Zhao, ZhiYong Su, Tong An, XingDuo Qin, JiaYang Gao</i>	
0024	182
MASS FRACTION CHECKS OF AN R1233ZD(E) AND R1234YF MIXTURE IN A HIGH-TEMPERATURE HEAT PUMP	
<i>Leon P. M. Brendel*, Silvan N. Bernal, Cordin Arpagaus, Sidharth Paranjape, Stefan S. Bertsch</i>	
0025	190
THERMALDYNAMIC ANALYSIS OF LOW GWP ALTERNATIVES IN HIGH TEMPERATURE HEAT PUMP: HFO1336mzz(Z) AND HFO1233zd(E)	
<i>Meng Yang, Hua zhang, Yanbin Qin, Kaifei Nong</i>	
0026	198
PERFORMANCE ANALYSIS FOR R1234ze(E) USING IN VAPOR INJECTED HIGH TEMPERATURE HEAT PUMP WITH FLASH TANK	
<i>Zhao Panpan, Jia Lei, Zhou Junhai, Qu boyi, Ke Yao, Wang Rujin</i>	
0027	206
CORRELATION FOR THERMAL CONDUCTIVITY OF HFOS AND HFO/HFC MIXTURES BASED ON FRICTION THEORY	
<i>Heyu Jia, Yu Hu, Yujing Zhang, Xiaopo Wang</i>	
0028	214
SURFACE TENSION OF 3,3,3-TRIFLUOROPROPENE/LUBRICANT MIXTURES FROM 283 K TO 343K	
<i>Heyu Jia, Yujing Zhang, Xiaopo Wang</i>	
0029	221
ANALYSIS ON THE APPLICATION OF AIR CYCLE HEAT PUMP SYSTEM WITH COMPRESSED NATURAL GAS PRESSURE POTENTIAL ENERGY RECOVERY FOR HIGH TEMPERATURE HEATING UNDER LOW AMBIENT TEMPERATURE CONDITIONS	
<i>Binfei Zhan, Zhichao Wang, Shuangquan Shao, Zhaowei Xu, Yingxia Yang, Jiandong Li, Xiaoxi Gou</i>	
0030	228
CONDENSATION HEAT TRANSFER OF R1233ZD(E) IN MICROCHANNELS	
<i>Jionghui LIU, Nan HUA, XinYu YOU, Yu XIA, Dilara SUULKER, Ji WANG, RongJi XU, GuangXu YU, HuaSheng WANG</i>	

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INFLUENCE OF SUBCOOLING IN R449A SUPERMARKET LOW-TEMPERATURE REFRIGERATION CIRCUIT USING MEDIUM TEMPERATURE COOLING LOAD

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ABSTRACT

This work studies the impact of subcooling in supermarket refrigeration systems with medium and low-temperature requirements based on a vapor compression single-stage with a subcooler. The energy performance (measured by the coefficient of performance, COP) of the low-temperature circuit has been analyzed considering the current system (with subcooling) and compared with a semi-empirical scenario without a subcooler. For a fixed cooling capacity, the new design compressors selected for R-449A reduce the compressor power consumption compared to the measurements, increasing COP, particularly at low-temperature lifts. Among the subcooler and no subcooler options, the differences are negligible in overall COP because the differences in COP for each stage are compensated. Carbon emissions calculated with the total equivalent warming impact (TEWI) are slightly lower in the configuration without a subcooler. From an energy and environmental point of view, it is not advisable to use subcooling in R-449A supermarket refrigeration.

Keywords: HFO mixtures, Commercial Refrigeration, Global Warming Potential (GWP), COP, Subcooler, R404A replacement

1. INTRODUCTION

Cold chain is essential for food conservation and freezing while keeping the maximum standards and avoiding the growth of bacteria. However, 12% of food in 2017 (526 Mt) was lost due to an insufficient cold chain or refrigeration (Sarr et al., 2021). In the current cold chain, most carbon emissions (60%) originate from refrigeration equipment's electricity consumption (261 MtCO_{2e}). An improved cold chain with significantly lower food losses would increase these emissions to 589 MtCO_{2e}. Therefore, highly energy-efficient equipment is required for commercial refrigeration.

Mota-Babiloni et al. (2022) proposed advanced configurations in a supermarket refrigeration unit operating with R-404A and retrofitted to R-449A. Parallel compression is the configuration that results in higher COP, but a simple retrofit to lower GWP refrigerants was the most convenient option. Citarella et al. (2022) demonstrated that R449A refrigerants perform better for mid-term commercial refrigeration in the European market. The optimal configuration in terms of energy performance has not the lowest environmental impact. Llopis et al. (2020) proposed a novel TEWI methodology considering the dependence of energy consumption with charge evolution and studied the impact on commercial refrigeration.

Cui et al. (2020) analyzed CO₂ booster configurations and three reference systems from energy, economic and environmental perspectives. Considering the results, CO₂ booster configurations are recommended for northern China. Still, the most advanced solution in Europe is unsuitable for China's hot climate cities, where R134a/CO₂ cascade refrigeration system can be considered a short-term solution. Giunta and Sawalha (2021) demonstrated that a supermarket based on CO₂ refrigeration could save up to 18% of the annual CO_{2e} emissions of the supermarket and increase benefits to 16% of the annual energy cost by selling part of the heat recovered to the district heating network operator. Karampour and Sawalha (2018) concluded that two-stage heat recovery, parallel compression, AC integration, and flooded evaporation are important improvements for CO₂ refrigeration systems. Mechanical

sub-cooling and gas cooler evaporative cooling are technologies considered arbitrary because of their impact and limitations.

Regarding mechanical subcooling, (Llopis et al., 2018) found benefits for CO₂ transcritical refrigeration. Regarding external subcooling methods, they highlighted dedicated mechanical subcooling. In this configuration, an auxiliary vapour compression system subcools the refrigerant at the condenser outlet before entering the expansion valve. The auxiliary system operates with a reduced temperature lift between the cold source and hot sink, reaching high COP values. Among other works, (Nebot-Andrés et al., 2022) compared this technology with other proposals for transcritical CO₂ refrigeration. Experimental tests validated the energy increase of the mechanical subcooling cycle compared to parallel compression. (ERDINC, 2022) proposed an expander-compressor booster-enhanced subcooling vapor compression cycle and compared R134a, R1234yf, R32, R290, R1270, and R600a.

(She et al., 2018) reviewed several works considering mechanical subcooling that concluded with COP benefits. (Qureshi and Zubair, 2012) investigated refrigerant combinations in dedicated mechanical subcooling vapor compression cycles. R134a caused the best results concerning COP, COP gain and relative compressor sizing in basic cycle and when dedicated mechanical subcooling is considered. In retrofit cases, dedicated mechanical subcooling is more suited to R134a as the main cycle because it has a negligible influence on the performance parameters when changing to the subcooler cycle. Besides, a subcooler between the medium-temperature (MT) refrigeration system and the low-temperature (LT) refrigeration system can be used for energy saving (Yang and Zhang, 2011). Optimal subcooler size and subcooling control increase energy savings of a two-temperature supermarket refrigeration system to 27% or 20% using R404A or R134a, respectively.

(Qureshi and Zubair, 2013) indicated the need for experimental work on residential, commercial, and industrial refrigeration equipment needs to the integrated subcooling cycle. This paper proposes a semi-empirical investigation of integrating subcooling units in an indirect supermarket refrigeration unit operating with R449A.

2. METHODS

2.1 Baseline

The supermarket refrigeration system is described in (Makhnatch et al., 2017), medium-temperature refrigeration units, and (Makhnatch et al., 2018), low-temperature refrigeration units. These works study both systems separately, analyzing the operational and energy performance when using R404A and R449A as a drop-in (or light retrofit) replacement. Figure 1 shows the schematic diagram and thermal and hydraulic connections between these circuits. All information necessary for describing the systems is included in the abovementioned papers.

The operation of the supermarket refrigeration unit (temperatures, pressures, compressor power consumption) was measured for an extended period using both refrigerants. Previous papers published have analyzed the energy and operational performance of the unit. The main conclusion was that R449A retrofit is beneficial in terms of operation, energy and environment. According to this, Mota-Babiloni et al. (2022) previous work confirms the economic advantage of the R449A light retrofit compared to the R404A baseline. As R449A supermarket refrigeration benefits have already been confirmed, this cycle is taken as the reference, SM, in the rest of the work. The steady-state operation of this unit will be considered as inputs (evaporation and condensation temperature) for the model developed to determine the semi-empirical operation.

2.2 Simulation strategy

Different scenarios are analyzed in this paper, considering the supermarket operation mentioned in the previous subsection as a baseline, keeping R449A as the refrigerant and selecting new compressors: 'SC' configuration for the simulation using MT evaporator to provide LT subcooling (initial cycle design), 'no SC' configuration for the simulation without a subcooler. Both cycles operate independently, and no subcooling is provided by a subcooler, liquid-to-suction heat exchanger, or any other means.

No SC configuration removes the LT subcooling provided by the MT units; therefore, new compressors are required to provide lower cooling capacity in the MT cycle and higher cooling capacity in the LT cycle. The same software for compressor selection has been used in the cycle with subcooling 'SC' to result in comparable compressor technology, response, and efficiencies.

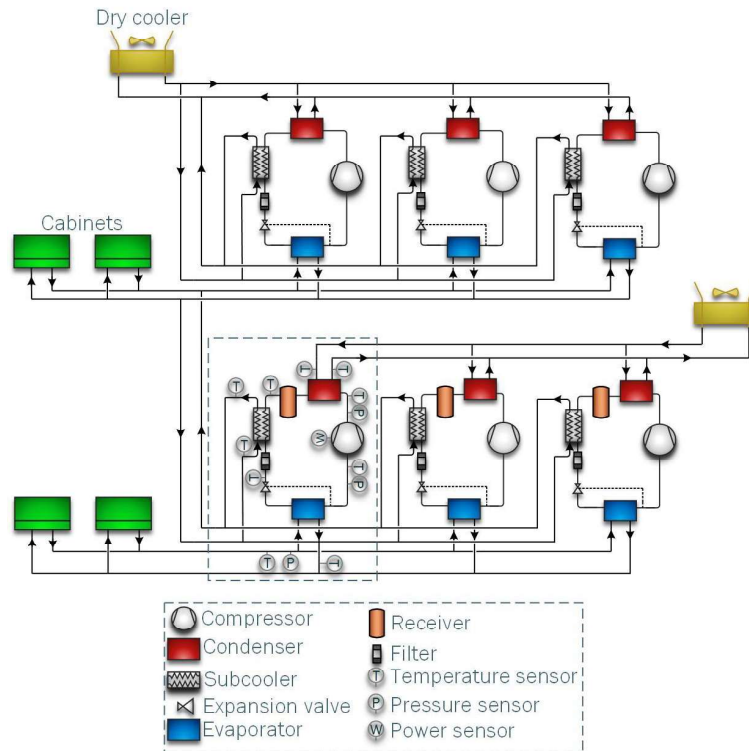


Figure 1: Supermarket refrigeration system schematic diagram

Thermodynamic states of refrigerants have been calculated using REFPROP v10.0. Basic vapor compression cycles have been simulated using MT and LT cooling capacity, evaporation, and condensation temperatures. For the simulation of the compressor efficiencies, subsection 2.3 exposes the methodology followed.

2.3 Compressor selection and simulation

The compressor selection is carried out using the current version of BITZER software (v6.17.9rev2794). As in the original system, semi-hermetic reciprocating compressors have been chosen. Each circuit's average cooling capacity and operational temperatures (evaporation and condensation) and scenario have been used as input. The resulting compressor models and main details can be seen in Table 1, where it can be extracted that 4 kW is the cooling load transferred in the subcooler. Moreover, when the subcooling is removed, the MT compressor volume displacement is reduced by 18% (6 cylinders instead of 8).

Table 1: Details of compressors included in the simulation

Circuit and scenario	Cooling load	Compressor model	Volume displacement (1450rpm at 50Hz)
MT SC	74 kW	8GE-60Y	185 m ³ h ⁻¹
LT SC	12.5 kW	4GE-23Y	84.5 m ³ h ⁻¹
MT no SC	70 kW	6FE-44Y	151.6 m ³ h ⁻¹
LT no SC	16.5 kW	4FE-28Y	101.8 m ³ h ⁻¹

In Table 2, equations required for determining the compressors' volumetric and isentropic efficiency are calculated through regressions depending on the evaporation and condensation temperatures. A high agreement (R^2) is observed between the correlations and the data provided by the compressor selection software. Besides isentropic and volumetric efficiencies, the electromechanical efficiency for the compressor-motor set is considered that of the IE4 motors (0.94 for MT and 0.92 for LT).

Table 2: Volumetric and isentropic compressor efficiency of simulated compressors

System	Equation	R ²
MT SC	$\eta_{vol} = 1.0328 + 0.00527 T_o - 0.00553 T_k$	0.99
	$\eta_{is} = 0.4353 - 0.00799 T_o + 0.0072 T_k - 0.0000625 T_o^2 - 0.00006525 T_k^2 + 0.000$	0.99
LT SC	$\eta_{vol} = 1.1827 + 0.00955 T_o - 0.00592 T_k$	0.94
	$\eta_{is} = 0.3398 - 0.01624 T_o + 0.01044 T_k - 0.0002587 T_o^2 - 0.0001282 T_k^2 + 0.000$	0.92
MT no SC	$\eta_{vol} = 1.0339 + 0.00473 T_o - 0.00438 T_k$	0.99
	$\eta_{is} = 0.4363 - 0.009371 T_o + 0.008621 T_k - 0.0001226 T_o^2 - 0.00008358 T_k^2 + 0.$	0.99
LT no SC	$\eta_{vol} = 1.1658 + 0.00902 T_o - 0.00591 T_k$	0.92
	$\eta_{is} = 0.3281 - 0.01613 T_o + 0.01143 T_k - 0.000243 T_o^2 - 0.0001292 T_k^2 + 0.0001$	0.91

2.4 Equations

The coefficient of performance of each cycle is calculated as indicated in Eq. (1). For the overall COP, the cooling capacity delivered to the refrigerated and frozen cabinets are summed, and divided by the sum of compressor power consumption.

$$COP = \frac{\dot{Q}_{evap}}{P_{el}} \quad \text{Eq. (1)}$$

$$COP_{overall} = \frac{\sum \dot{Q}_{evap}}{\sum P_{el}} \quad \text{Eq. (2)}$$

3. RESULTS

3.1 Energy performance

This section shows the COP measured and simulated in the proposed configurations. Figure 2 shows the COP of individual cycles for MT and LT stages. Given that the simulation uses evaporation and condensation temperatures and cooling capacity as input, COP results in the simulation are less scattered. However, the trend at hightemperature lift is comparable for MT, and at all conditions for LT.

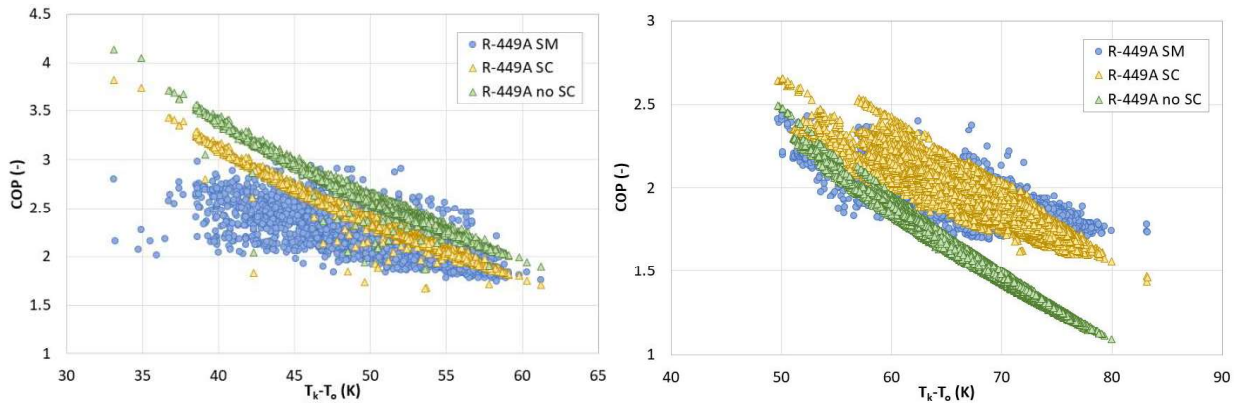


Figure 2: COP of MT (left) and LT (right) circuits

Regarding the MT circuit, the average COP values for SM, SC and no SC are 2.20, 2.30, and 2.53, respectively. The new compressor increases the COP if SC and SM are compared. Then, the no SC situation results in higher COP because all the cooling capacity is used in the same cycle. The model can be considered highly accurate for the LT circuit as SM and SC COP values are comparable, 1.88. For the no SC scenario, the average COP is 1.47. This reduction is because of the removal of subcooling, so all the cooling capacity must be provided by a higher mass flow rate, which increases the compressor power consumption and decreases COP.

For the energy performance simulation, the cooling capacity is fixed, so the difference in COP is caused by compressor power consumption. Figure 3 shows the resulting compressor power consumption. In the MT circuit, as the SC configuration requires a higher cooling capacity to provide refrigeration to frozen cabinets and LT

subcooler, the mass flow rate is higher and increases the compressor power consumption. The contrary occurs in the LT circuit, as explained above. The average compressor power consumption values for the MT circuit are 34.1, 33.2 and 27.9 kW for SM, SC, and no SC configurations, respectively. Then, concerning the LT circuit, the average compressor power consumption values are 8.8, 8.9 and 10.6 kW for SM, SC, and no SC configurations, respectively.

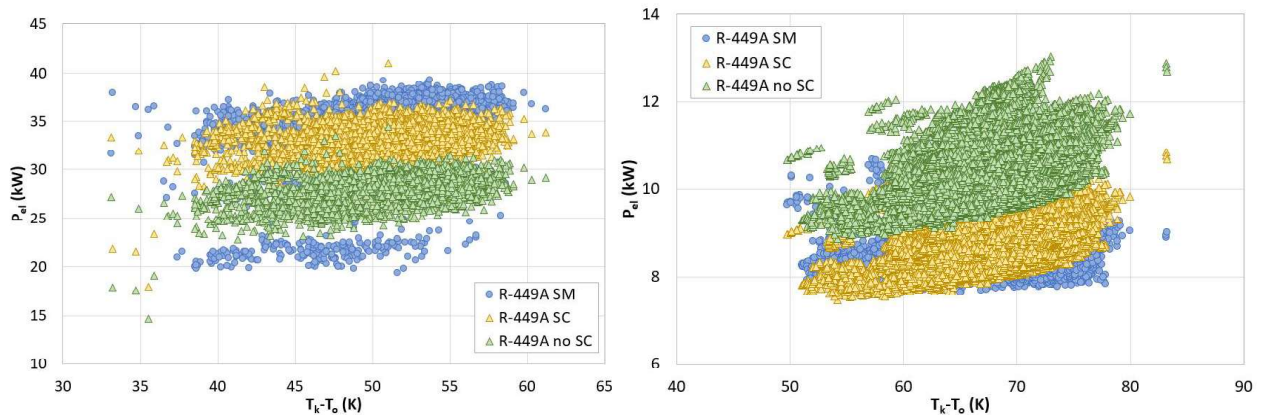


Figure 3: Compressor power consumption of MT (left) and LT (right) circuits

The overall COP is calculated to determine the energy benefit of the supermarket refrigeration system, Figure 4. The axes represent the temperature lifts for each circuit. At high temperature lifts, the three configurations show a comparable overall COP value. Contrarily, for low temperature lifts, the SM configuration performs below simulations using new design compressors. Comparing SC and no SC configurations, the overall COP is comparable for most conditions, being slightly higher for the no SC configuration at low temperature lifts.

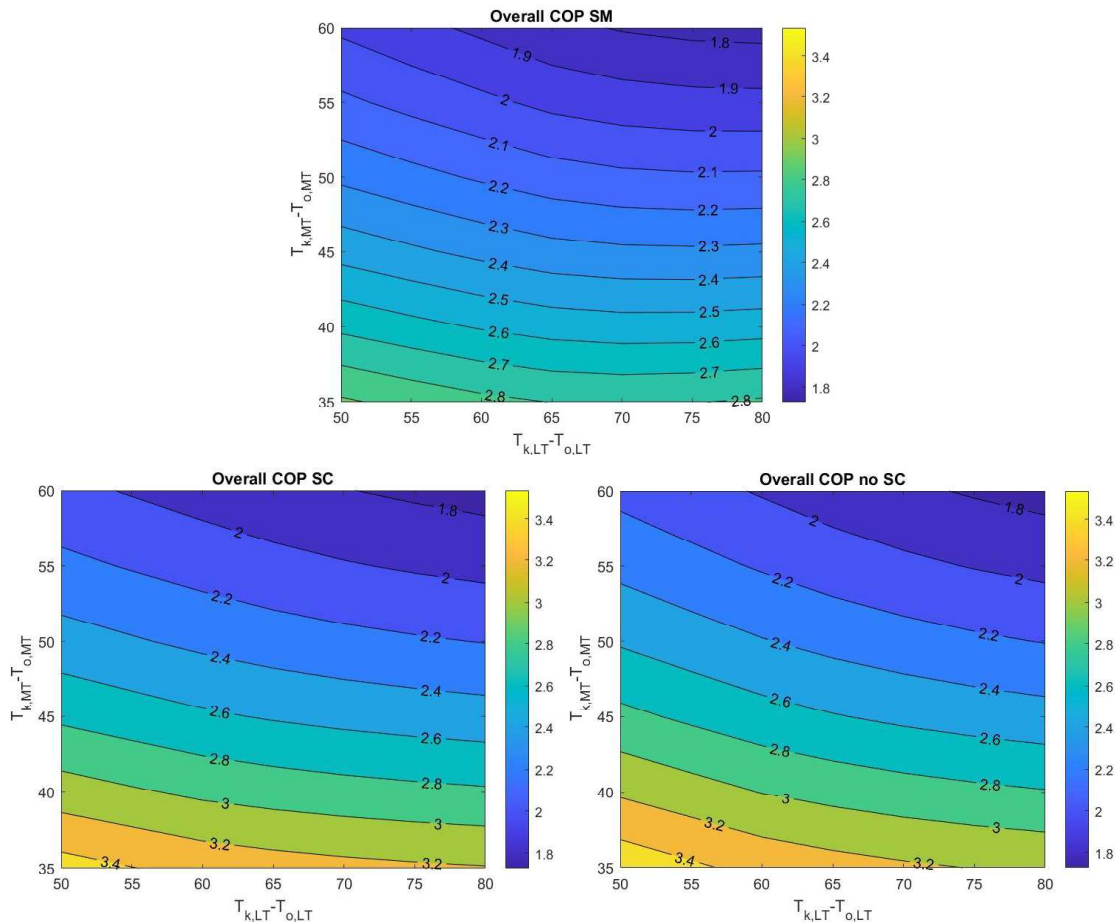


Figure 4: Overall COP for SM (top), SC (down left) and no SC (down right) circuits

3.2 Carbon footprint assessment

The total equivalent warming impact (TEWI) is used as the indicator for the carbon footprint. Indications provided by (Mota-Babiloni et al., 2020) have been followed. For the TEWI, the refrigerant charge in the subcooler is calculated with the SWEP design software because it is removed for the no SC configuration. The measured and simulated compressor power consumption has been extended over a year. TEWI has been calculated for the whole unit, considering the 3 circuits for MT and another 3 for LT. As the baseline supermarket was located in Sweden, the Swedish carbon emission factor is taken, $0.0088 \text{ kgCO}_2\text{e kWh}^{-1}$. Figure 5 shows the TEWI results indicating the type of carbon emissions. A new design compressor can reduce carbon emissions over the SM solution. Then, as the no SC configuration requires less refrigerant charge and the COP was slightly higher, both direct and indirect emissions are reduced.

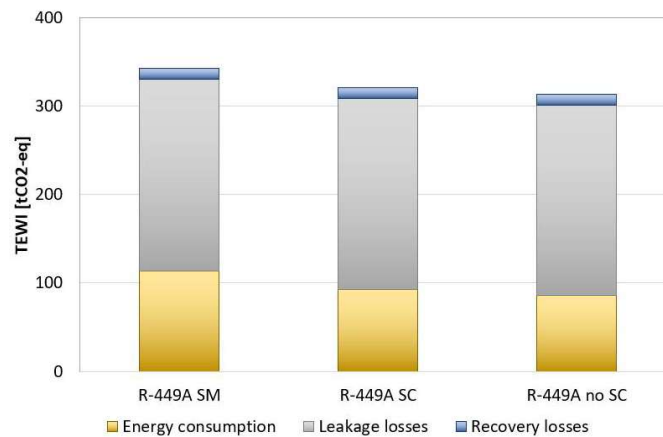


Figure 5: TEWI

4. CONCLUSIONS

Subcooling can translate cooling capacity from an MT circuit to an LT. This is a common practice because supermarket refrigeration systems usually present a higher cooling capacity in the MT circuit. This paper compares the options with and without a subcooler to determine the benefit based on a semi-empirical analysis. After selecting new compressors adjusted to the required cooling capacity, the energy analysis reveals that COP is comparable between both options and that the carbon footprint is lower without a subcooler.

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NOMENCLATURE

\dot{P}_{el}	Power consumption (kW)	<i>vol</i>	volumetric
T	temperature (°C)	<i>is</i>	isentropic
k	condensation	<i>o</i>	evaporation
COP	Coefficient of performance (-)	\dot{Q}_{evapor}	Cooling capacity (kW)

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